

## Solid-State Batteries

How to cite: *Angew. Chem. Int. Ed.* **2023**, 62, e202213228

International Edition: doi.org/10.1002/anie.202213228

German Edition: doi.org/10.1002/ange.202213228

# Impact of the Chlorination of Lithium Argyrodites on the Electrolyte/Cathode Interface in Solid-State Batteries

Tong-Tong Zuo,\* Felix Walther, Jun Hao Teo, Raffael Rueß, Yubo Wang, Marcus Rohnke, Daniel Schröder, Linda F. Nazar, and Jürgen Janek\*

**Abstract:** Lithium argyrodite-type electrolytes are regarded as promising electrolytes due to their high ionic conductivity and good processability. Chemical modifications to increase ionic conductivity have already been demonstrated, but the influence of these modifications on interfacial stability remains so far unknown. In this work, we study  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  to investigate the influence of halogenation on the electrochemical decomposition of the solid electrolyte and the chemical degradation mechanism at the cathode interface in depth. Electrochemical measurements, gas analysis and time-of-flight secondary ion mass spectrometry indicate that the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows pronounced electrochemical decomposition at lower potentials. The chemical reaction at higher voltages leads to more gaseous degradation products, but a lower fraction of solid oxygenated phosphorous and sulfur species. This in turn leads to a decreased interfacial resistance and thus a higher cell performance.

## Introduction

The demand for high energy density and safety accelerates the development of solid-state batteries (SSBs).<sup>[1]</sup> In order to meet the requirements of high energy and power density, solid electrolytes (SEs) with high ionic conductivity show great potential in satisfying these criteria.<sup>[2]</sup> Among all SEs, sulfide-based electrolytes exhibit particularly high ionic conductivity and favorable mechanical properties (e.g., high elasticity and ductility), which are important for practical processing of SSBs, especially for thick cathodes. A number of sulfide SEs have been studied including  $\text{Li}_2\text{S-P}_2\text{S}_5$  glasses,<sup>[3]</sup>  $\text{Li}_{10}\text{GeP}_2\text{S}_{12}$ ,<sup>[4]</sup>  $\text{Li}_{9.54}\text{Si}_{1.74}\text{P}_{1.44}\text{S}_{11.7}\text{Cl}_{0.3}$ ,<sup>[5]</sup> and  $\text{Li}_6\text{PS}_5\text{X}$  ( $\text{X} = \text{Cl}, \text{Br}, \text{I}$ ).<sup>[6]</sup> However, due to the rather limited thermodynamic stability of the thiophosphate and sulfide ions, most thiophosphate SEs exhibit a narrow electrochemical stability window, which is problematic in combination with high voltage cathode active materials (CAMs), such as  $\text{LiNi}_{1-x-y}\text{Co}_x\text{Mn}_y\text{O}_2$  (NCM).<sup>[7]</sup> Recently, a spate of Li metal halide SEs have been studied intensively, as they provide much better cathode compatibility and high voltage stability, however, their ionic conductivity is still lower than that of optimized sulfide SEs.<sup>[8]</sup>

Lithium argyrodites with the formula  $\text{Li}_6\text{PS}_5\text{X}$  ( $\text{X} = \text{Cl}, \text{Br}, \text{I}$ ) show great advantages owing to their outstanding processability and high ionic conductivity.<sup>[9]</sup> Kraft et al. systematically studied the influence of the different halide anions ( $\text{Cl}^-$ ,  $\text{Br}^-$ , and  $\text{I}^-$ ) on the ionic conductivity.<sup>[6c]</sup> Upon altering the lattice softness of Li argyrodites, the ionic transport was investigated via monitoring the  $\text{Li}^+$  occupancy and  $\text{X}^-/\text{S}^{2-}$  site disorder. It was shown that the compositional change of the halide triggers the change of site disorder due to the characteristic properties of different halide anions. Recently, Gautam et al. controlled the site-disorder in  $\text{Li}_6\text{PS}_5\text{Br}$  by tuning the synthesis temperature before quenching.<sup>[10]</sup> The results suggest that a higher degree of site disorder is beneficial for intercalation jumps, and leads to a fourfold increase in ionic conductivity to  $2 \text{ mS cm}^{-1}$ . Apart from the compositional change of the halide, increasing the halide content from  $\text{Li}_6\text{PS}_5\text{Cl}$  to  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  also introduces more  $\text{Li}^+$  vacancies and  $\text{Cl}^-/\text{S}^{2-}$  site disorders.<sup>[11]</sup> Owing to the weakened interaction between Li ions and the surrounding framework, the Cl-rich argyrodite  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows an enhanced ionic conductivity of  $12 \text{ mS cm}^{-1}$  when pelletized and sintered. Clearly, the ionic conductivity of the Li argyrodites has been greatly improved, but the impact of the chemical modification on the stability and interfacial degra-

[\*] Dr. T.-T. Zuo, Dr. F. Walther, Dr. R. Rueß, Prof. M. Rohnke, Prof. J. Janek  
 Institute of Physical Chemistry, Justus Liebig University Giessen  
 Heinrich-Buff-Ring 17, 35392 Giessen (Germany)  
 and  
 Center for Materials Research (ZfM/LaMa),  
 Justus Liebig University Giessen  
 Heinrich-Buff-Ring 16, 35392 Giessen (Germany)  
 E-mail: tong-tong.zuo@phys.chemie.uni-giessen.de  
 juergen.janek@pc.jlug.de

J. H. Teo  
 Battery and Electrochemistry Laboratory, Institute of Nanotechnology,  
 Karlsruhe Institute of Technology (KIT)  
 Hermann-von-Helmholtz-Platz 1,  
 76344 Eggenstein-Leopoldshafen (Germany)

Y. Wang, Prof. L. F. Nazar  
 Department of Chemistry and the Waterloo Institute for Nanotechnology,  
 University of Waterloo  
 200 University Avenue West, Waterloo, Ontario N2L 3G1 (Canada)  
 Prof. D. Schröder  
 Institute of Energy and Process Systems Engineering (InES),  
 Technische Universität Braunschweig  
 Langer Kamp 19B, 38106 Braunschweig (Germany)

© 2022 The Authors. Angewandte Chemie International Edition published by Wiley-VCH GmbH. This is an open access article under the terms of the Creative Commons Attribution Non-Commercial NoDerivs License, which permits use and distribution in any medium, provided the original work is properly cited, the use is non-commercial and no modifications or adaptations are made.

dation at the SE|CAM interface has not been studied in depth.

Recently, Dewald et al. and Tan et al. investigated the practical oxidative stability of  $\text{Li}_6\text{PS}_5\text{Cl}$  with carbon electrodes.<sup>[7b,12]</sup> The oxidation of sulfide ( $\text{S}^{2-}$ ) in the thiophosphate polyanions to sulfur ( $\text{S}_x^0$  and  $\text{S}_x^{2-}$  species) dominates the electrochemical decomposition of the SE, representing lithium extraction. However, in contact with the cathode active material (CAM), the formation of oxygenated sulfur and phosphorous species indicates additional chemical degradation at the CAM|SE (e.g.,  $\text{Li}_6\text{PS}_5\text{Cl}$ | $\text{LiNi}_{0.6}\text{Co}_{0.2}\text{Mn}_{0.2}\text{O}_2$ ) interface.<sup>[13]</sup> Furthermore, the observation of gaseous products (e.g.,  $\text{SO}_2$ ) indicates the reaction between  $\text{O}_2$  (presumably singlet  $^1\text{O}_2$ <sup>[14]</sup>) released from the NCM with  $\text{Li}_6\text{PS}_5\text{Cl}$ .<sup>[15]</sup> These results highlight that both electrochemical decomposition of the SE and its chemical reactivity with the CAM play a critical role and need to be taken into account on the way to optimized interfaces for SSBs.

In this work, we employ  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  electrolytes as a model system in which the increased halide content affects the ionic conductivity without major structural changes. The electrochemical and chemical stability of the SE is measured in SE/carbon and SE/CAM composite electrodes, respectively.  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows more pronounced decomposition at the interface with both carbon and CAM. Time-of-flight secondary-ion mass spectrometry (ToF-SIMS) and differential electrochemical mass spectrometry (DEMS) were carried out to probe the solid and gaseous degradation products. In comparison with  $\text{Li}_6\text{PS}_5\text{Cl}$ ,  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  yields more products containing elemental sulfur (i.e.,  $\text{S}_x^0$  and polysulfides  $\text{S}_x^{2-}$ ) and more gas (i.e.,  $\text{SO}_2$ ), but it forms less solid oxygenated sulfur and phosphorus compounds (i.e., phosphate and sulfate/sulfite). Accordingly, the SE modification leads to changes in the underlying interfacial reactions and thus differences in the fractions of the various cathode|electrolyte interphase (CEI) compounds. A thin and homogeneous lithium phosphate/phosphite or lithium sulfate/sulfite layer in turn improves the cell performance in the case of  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ . Overall, these findings provide new insights into the influence of electrolyte modification on cathode interfacial stability.

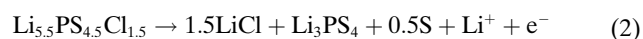
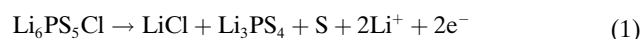
## Results and Discussion

$\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  electrolytes were prepared by a well-known solid-state synthesis route as reported elsewhere.<sup>[11a]</sup> Figure S1 shows the XRD patterns of  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  powders. The reflections at  $2\theta$  positions  $35^\circ$  and  $50^\circ$  indicate a very minor LiCl impurity in  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ , while no impurities are found in  $\text{Li}_6\text{PS}_5\text{Cl}$ . The ionic conductivity at  $25^\circ\text{C}$  was measured to be  $2.9\text{ mS cm}^{-1}$  for  $\text{Li}_6\text{PS}_5\text{Cl}$ , whereas  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows a higher conductivity of  $7.0\text{ mS cm}^{-1}$ , which is in good agreement with the literature value.<sup>[11a]</sup>

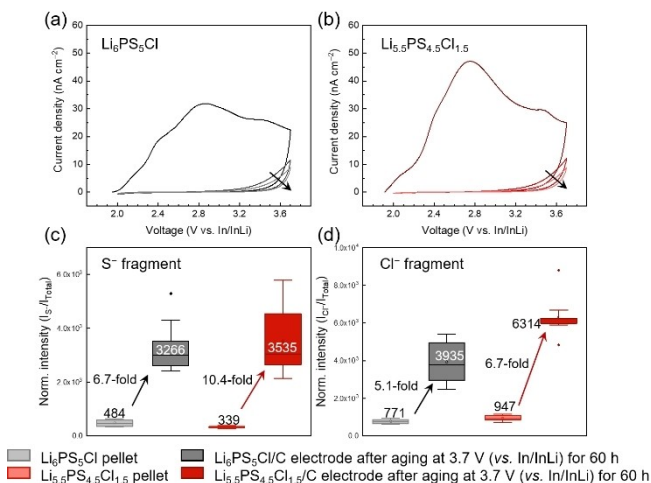
In order to determine the electrochemical stability window of both SEs, cyclic voltammetry (CV) measure-

ments were performed with carbon electrodes. Figure 1a and b show the CV results of the  $\text{Li}_6\text{PS}_5\text{Cl}/\text{C}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrodes, respectively. At a scan rate of  $0.05\text{ mV s}^{-1}$ , the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrode exhibits an approximately twofold higher current density compared with the  $\text{Li}_6\text{PS}_5\text{Cl}/\text{C}$  electrode, while all maxima appear at the same potentials (Figure S2). Under the assumption that both electrolytes are equally well in contact with the carbon, this result indicates that a)  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  is more susceptible to electrochemical decomposition than  $\text{Li}_6\text{PS}_5\text{Cl}$ , and that b) the oxidation mechanism is similar.

The electrochemical decomposition of thiophosphate SEs has been widely investigated experimentally and computationally.<sup>[7b,12,16]</sup> Theoretically, Li argyrodite SEs decompose first into  $\text{LiCl}$ ,  $\text{Li}_3\text{PS}_4$  and S (more correctly  $\text{S}_x^0$  and/or  $\text{S}_x^{2-}$ , depending on the degree of oxidation) upon oxidation [Reactions (1) and (2)], subsequently  $\text{Li}_3\text{PS}_4$  decomposes into S and  $\text{P}_2\text{S}_5$  after complete oxidation [Reaction (3)].



Reactions (1)–(3) are highly simplified as the underlying decomposition processes are mechanistically rather complex, involving a large variation of possible intermediate products (e.g.,  $\text{PS}_4^{3-}$ ,  $\text{P}_2\text{S}_7^{4-}$ , and  $\text{P}_2\text{S}_6^{2-}$ ).<sup>[7b]</sup> However, following these



**Figure 1.** CV measurements of a)  $\text{In}/\text{InLi}|\text{Li}_6\text{PS}_5\text{Cl}|\text{Li}_6\text{PS}_5\text{Cl}/\text{C}$  and b)  $\text{In}/\text{InLi}|\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}|\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  cells at  $25^\circ\text{C}$ . The content of C additive is 20 wt%. The surface area of C65 was measured to be  $59\text{ m}^2\text{ g}^{-1}$ . We assume that all carbon particles are well covered by SEs in the SE/C electrode. The arrows indicate the CV curves from the first to the third cycle. Box plots of normalized c)  $\text{S}^-$  and d)  $\text{Cl}^-$  signal intensities of ToF-SIMS surface analyses (10 measurements per sample) of SE/C electrodes. The signal intensity is normalized to the total ion signal intensity of the corresponding spectrum. The average signal intensities were labelled in (c) and (d). The relative increase of  $\text{S}^-$  and  $\text{Cl}^-$  signal intensities were evaluated to compare the decomposition degree of SEs.

equations for sake of simplicity, the complete decomposition process of the SE should involve  $5e^-$  per formula unit for  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $4e^-$  per formula unit for  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ . Consequently, the higher current density in the CV measurements could be explained either by a higher fraction of decomposed SE material or by a “more complete” decomposition process.

In contrast to  $\text{Li}_6\text{PS}_5\text{Cl}$ , a lower oxidation onset is found for  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  (Figure S2). This correlates with its thermodynamically unstable nature determined from differential scanning calorimetry (DSC) and thermal gravimetric analysis (TGA) measurements. In the DSC measurement (Figure S3a), sharp melting/crystallization peaks were observed for  $\text{Li}_6\text{PS}_5\text{Cl}$  at  $535^\circ\text{C}/532^\circ\text{C}$ , respectively. For  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ , the melting/crystallization peaks become broader and shift to lower temperature ( $523^\circ\text{C}/493^\circ\text{C}$ ), which may indicate incongruent melting. The TGA curves show no significant mass loss for  $\text{Li}_6\text{PS}_5\text{Cl}$ , but for  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ , the mass starts to drop at  $315^\circ\text{C}$  (Figure S3b). The underlying reactions during heating remain elusive. Nevertheless, both DSC and TGA experiments demonstrate the thermodynamic instability of  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ , which leads to a larger driving force towards decomposition in electrochemical measurements.

The galvanostatic intermittent titration technique (GITT) was applied to investigate the voltage-dependence on the electrochemical decomposition. Upon polarization, the sharp voltage increase (IR drop) reflects the internal resistance in the cell (Figure S4a). In the low voltage range ( $<3\text{ V}$  vs.  $\text{In}/\text{InLi}$ ), the internal resistance of cells with either  $\text{Li}_6\text{PS}_5\text{Cl}$  or  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  is almost the same, while the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrode exhibits higher capacity due to electrochemical decomposition. At voltages above  $3\text{ V}$  vs.  $\text{In}/\text{InLi}$ , the internal resistance of the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrode increases faster than the  $\text{Li}_6\text{PS}_5\text{Cl}/\text{C}$  electrode, and the two electrodes deliver similar decomposition capacity. This implies that the electrochemical decomposition is a voltage-dependent process, while it is difficult to correlate the IR drop with decomposition steps due to the lack of detailed compositions and their resistance.

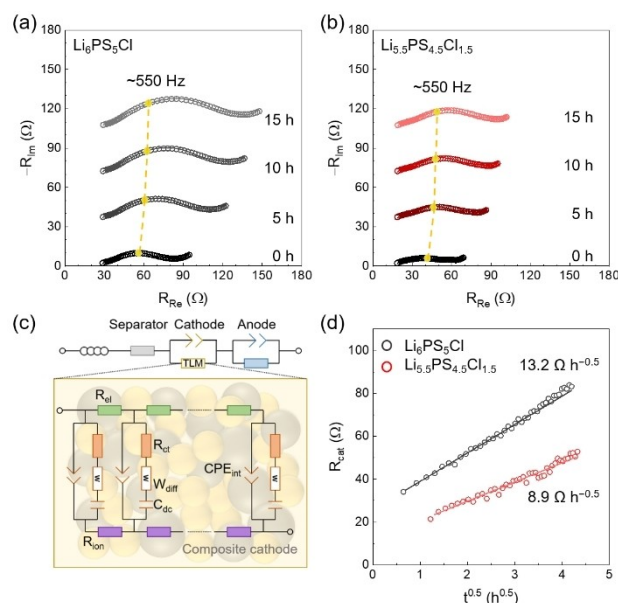
ToF-SIMS measurements were performed on the surface of SE/C electrodes (oriented towards the current collector) after holding the voltage at  $3.7\text{ V}$  vs.  $\text{In}/\text{InLi}$  for  $60\text{ h}$ . Figure 1c and d show the signal intensities of  $\text{S}^-$  and  $\text{Cl}^-$  secondary ions (normalized to the total ion signal intensity) for both SEs, respectively. Under the assumption that  $\text{S}^-$  and  $\text{Cl}^-$  are more easily formed from decomposition products (due to higher fragmentation), the strong increase in normalized signal intensities is correlated to the decomposition of both argyrodite materials upon electrochemical oxidation. For  $\text{Li}_6\text{PS}_5\text{Cl}$ , the normalized intensity of the  $\text{S}^-$  signal is similar to  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  in the pristine pellet as well as after aging. On the contrary, the intensity of the normalized  $\text{Cl}^-$  signal is higher in the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrode after aging. The effect of the current collector on the decomposition reaction is not clear, but this may offset the difference in  $\text{S}^-$  and  $\text{Cl}^-$  signal intensities to some extent.<sup>[17]</sup>

Based on the Reactions (1)–(3), the chemical stoichiometry of the Li argyrodite determines the ratio of the

decomposition products. Considering the relative intensity changes of the  $\text{S}^-$  (6.7- : 10.4-fold increase for  $\text{Li}_6\text{PS}_5\text{Cl}:\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ ) and  $\text{Cl}^-$  (5.1- : 6.7-fold increase for  $\text{Li}_6\text{PS}_5\text{Cl}:\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ ) signals and the observations on the current density of SE/C electrodes, we speculate that the fraction of decomposition products in the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{C}$  electrode is higher than in the  $\text{Li}_6\text{PS}_5\text{Cl}/\text{C}$  electrode. In other words,  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows a higher degree of electrochemical decomposition.

To quantify the interfacial degradation at the SE|NCM85 interface,  $\text{Li}_6\text{PS}_5\text{Cl}/\text{NCM85}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM85}$  cells were charged up to  $3.7\text{ V}$  vs.  $\text{In}/\text{InLi}$  and held at this voltage, while impedance spectra were measured every  $25\text{ min}$  for  $30\text{ h}$ . Figure 2a, b show that the resistance of the two cells increases strongly during aging. A transmission line model (TLM) was applied to extract the charge transfer and the electronic/ionic transport processes in the composite cathodes (Figure 2c).<sup>[18]</sup> As the impedance shows a typical Gerischer-type behavior, the charge transfer and transport resistances cannot be accurately decoupled from each other by fitting. However, an effective total resistance of the composite cathode can be determined as:<sup>[18e]</sup>

$$R_{\text{cat}} = \sqrt{R_{\text{ct}}(R_{\text{el}} + R_{\text{ion}})} \quad (4)$$



**Figure 2.** Impedance evolution of a)  $\text{Li}_6\text{PS}_5\text{Cl}$  and b)  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  SSBs resting upon  $3.7\text{ V}$  vs.  $\text{In}/\text{InLi}$  at  $25^\circ\text{C}$ . The impedance spectra are stacked with a y-axis shift of  $35\ \Omega$  for each spectrum. The equivalent circuit and the corresponding contributions are marked in (c). The transport-reaction scheme in the composite cathode is described by a transmission line model (TLM).  $R_{\text{ct}}$ ,  $R_{\text{el}}$  and  $R_{\text{ion}}$  represent the resistance contributions from charge transfer, electron transport and ionic transport, respectively.  $W_{\text{diff}}$  denotes the Warburg impedance for diffusion inside insertion active particle.  $C_{\text{dc}}$  accounts for the differential capacity of NCM.  $CPE_{\text{int}}$  represents the constant phase element for the interfacial capacitance. d) Comparison of  $R_{\text{cat}}$  increase against the square root of time ( $t^{0.5}$ ).



where  $R_{\text{cat}}$  denotes the overall cathode resistance.  $R_{\text{ct}}$ ,  $R_{\text{el}}$  and  $R_{\text{ion}}$  represent the resistance contributions from charge transfer, electron transport and ionic transport, respectively. Figure S5 displays the impedance evolution of the cathode and anode parts. The resistance contribution of the cathode side dominates the total resistance of the cell and increases parabolically over time. As shown in Figure 2d, the resistance of the  $\text{Li}_6\text{PS}_5\text{Cl}/\text{NCM85}$  composite cathode exhibits a steep square root increase with a rate constant of  $13.2 \Omega \text{h}^{-0.5}$ . In contrast, the resistance of the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM85}$  cathode increases parabolically with a rate constant of  $8.9 \Omega \text{h}^{-0.5}$ . This result suggests that the interfacial degradation of the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM85}$  composite cathode is slower, and we assume the following mechanism: first, electrochemical decomposition by extraction of lithium and oxidation of sulfur (without contribution of oxygen from the NCM) takes place on the NCM surface, analogous to the SE/C interface. Additionally, a chemical reaction of NCM and the SE can occur, which is probably accompanied by oxygen release from the NCM85 lattice at high voltages ( $>3.6 \text{ V vs. In/InLi}$ ). The highly reactive oxygen species can further react with the SE and leads to gaseous and oxygenated degradation products.<sup>[7c,19]</sup> Therefore, the parabolic increase in resistance shows a combined effect of electrochemical decomposition and chemical degradation.

To monitor the impedance evolution during cycling, full cells with NCM85 and different SEs were examined at  $0.96 \text{ mA cm}^{-2}$  ( $0.5 \text{ C}$ ). The  $\text{Li}_6\text{PS}_5\text{Cl}$  cell displays an initial charge and discharge capacity of 215 and  $165 \text{ mAh g}^{-1}$  (Figure 3a), while the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell exhibits an initial charge and discharge capacity of 215 and  $170 \text{ mAh g}^{-1}$  (Figure 3b), resulting in Coulombic efficiencies of 77 % and 79 %, respectively. After 50 cycles, the  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cells still show discharge capacities of 133 and  $145 \text{ mAh g}^{-1}$ , respectively. After each charging step, impe-

dance spectra was measured and fitted with the equivalent circuit (Figure 2c) to extract the cathode interfacial charge transfer processes in the cells. The increasing resistance during cycling is ascribed to the interfacial reactions at the SE|CAM interface (Figure S6). Upon cycling, the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell exhibits higher capacity than the  $\text{Li}_6\text{PS}_5\text{Cl}$  cell, but the differences in resistance increase of the two cells are insignificant. We note that the cells for the measurements shown in Figure 2 were held at  $3.7 \text{ V vs. In/InLi}$ —which would support the chemical degradation caused by oxygen release from the NCM85, whilst the electrochemical decomposition would be more pronounced during cell cycling as shown in Figure 3.

In addition, the morphological/structural degradation is typically more pronounced at higher cycle numbers. Assuming that the mechanical properties of both SEs are similar, morphological/structural degradation should be more or less comparable for both SSBs and should therefore contribute to a similar extent to the overall SSB performance at higher cycle numbers.

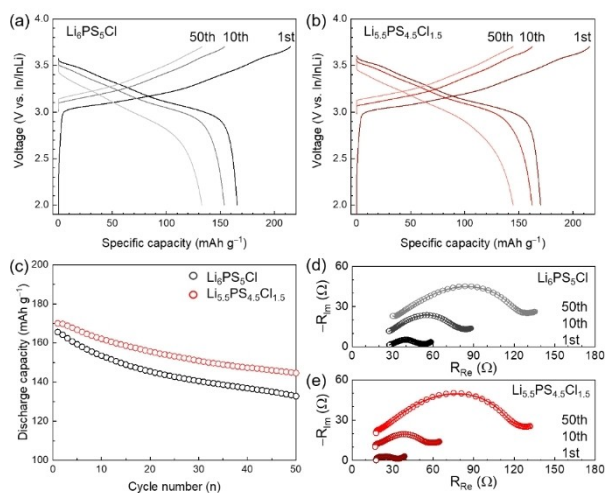
Given the different ionic conductivity for the different Li argyrodites, the transport kinetics in two composite cathodes were compared by rate experiments. As shown in Figure S5a,b,  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cells show initial discharge capacities of 183 and  $198 \text{ mAh g}^{-1}$  at  $0.1 \text{ C}$ , respectively. With increasing C-rate, the  $\text{Li}_6\text{PS}_5\text{Cl}$  cell exhibits gradually decaying discharge capacities of 165, 132, 96, and  $46 \text{ mAh g}^{-1}$  at 0.2, 0.5, 1 and  $2 \text{ C}$ , respectively. In contrast, the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell displays higher discharge capacities of 185, 160, 132, and  $85 \text{ mAh g}^{-1}$ . The obvious difference in rate capability could be ascribed to the higher ionic conductivity of  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ . On the one hand, the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  separator facilitates ion transport between electrodes with lower overvoltage. On the other hand,  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  offers a higher local ionic conductivity in the composite cathode. In order to deconvolute both contributions to the rate capability, four cells with the following separator|cathode combinations were examined:

$\text{Li}_6\text{PS}_5\text{Cl}$  SE| $\text{Li}_6\text{PS}_5\text{Cl}/\text{NCM}$  composite cathode

$\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  SE| $\text{Li}_6\text{PS}_5\text{Cl}/\text{NCM}$  composite cathode

$\text{Li}_6\text{PS}_5\text{Cl}$  SE| $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  composite cathode

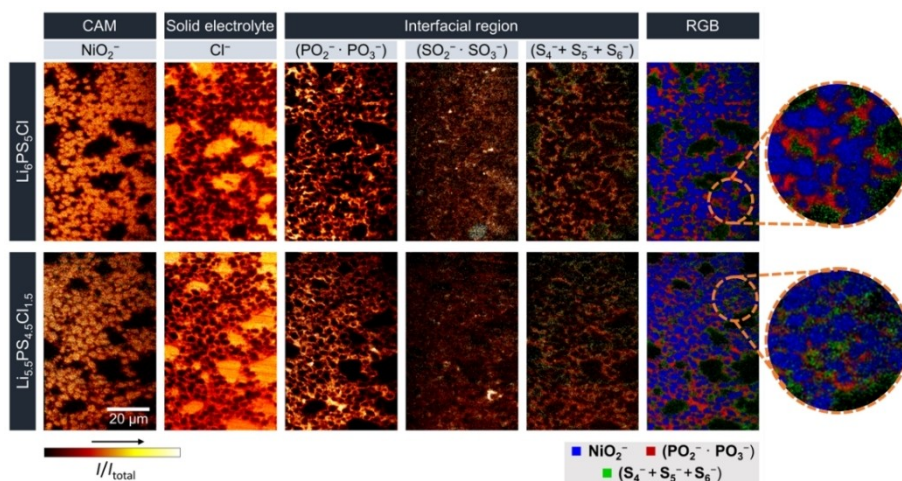
$\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  SE| $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  composite cathode



**Figure 3.** Galvanostatic charge/discharge curves of a)  $\text{Li}_6\text{PS}_5\text{Cl}$  and b)  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cells at  $0.5 \text{ C}$ . c) Comparison of the cycling stability of two cells. Nyquist plots of d)  $\text{Li}_6\text{PS}_5\text{Cl}$  and e)  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cells after 1st, 10th and 50th charge.

Figure S8 and Table S1 display the rate capability of the four cells. At low C-rate conditions ( $0.1 \text{ C}$  and  $0.2 \text{ C}$ ), the two cells with  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  cathodes exhibit higher capacity, while the two cells with  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  SEs show higher capacities at high C-rates. This implies that the limiting step is rooted in the composite cathode at low C rates, while the ionic conductivity of the SE separator dominates the rate capability at high C-rates. Obviously, the higher ionic conductivity of the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  SE is favorable for the construction of SSBs.

In order to investigate the interfacial degradation processes, ToF-SIMS surface analysis was carried out on the



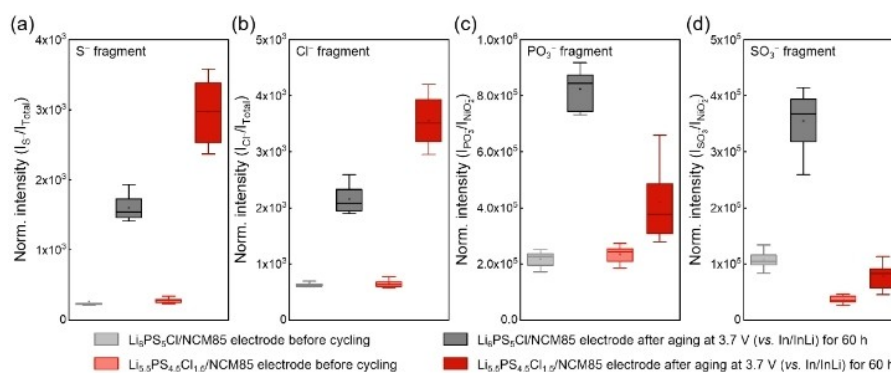
**Figure 5.** ToF-SIMS measurements of  $\text{Li}_6\text{PS}_4\text{Cl}/\text{NCM}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  cells after 100 cycles. All spectra were measured in negative ion mode on the sidewalls of  $45^\circ$  craters. All secondary ion images were normalized to the total ion signal to compensate topographic effects such as the FIB crater geometry. Exemplary of Supporting Information images of  $\text{NiO}_2^-$ ,  $\text{Cl}^-$ ,  $(\text{PO}_2^- \cdot \text{PO}_3^-)$ ,  $(\text{SO}_2^- \cdot \text{SO}_3^-)$ ,  $(\text{S}_4^- + \text{S}_5^- + \text{S}_6^-)$  and a RGB overlap. Cathode active material particles, solid electrolyte, and degradation layer are well distinguished in the overlay image.

side of the composite cathode (SE/NCM) that was oriented towards the current collector, after aging for 60 h at 3.7 V. The normalized intensities related to  $\text{S}^-$  and  $\text{Cl}^-$  increase strongly during aging for both electrodes (Figure 4a,b), suggesting electrochemical decomposition of both SEs (higher fragmentation of the SE). Assuming the microstructures in the composite cathodes are similar (Figure S9), the comparably higher intensities of the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  electrode after aging indicate more severe SE decomposition. Figure S10 presents the signal intensities of a series of polysulfide species ( $\text{S}_x^-$ ,  $1 \leq x \leq 4$ ). The increase in  $\text{S}^-$  intensity after aging is reflected as well in the  $\text{S}_2^-$  and  $\text{S}_3^-$  signals for the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  electrode. However, concerning the overlapping impact of current collectors,<sup>[17,20]</sup> the difference in two electrodes is gradually eliminated, especially for the  $\text{S}_4^-$  fragment.

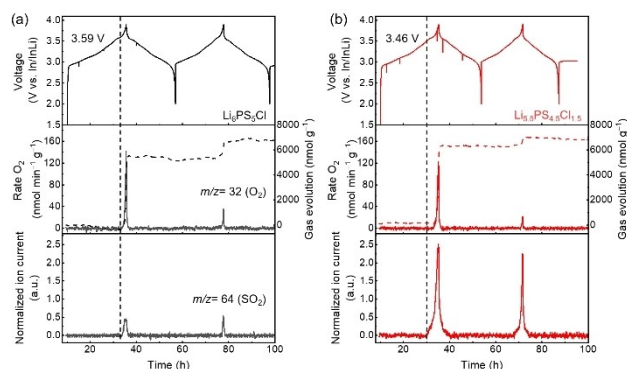
Due to the affinity of oxygen to react with phosphorus and sulfur, phosphate ( $\text{PO}_x^-$ ) and sulfite/sulfate ( $\text{SO}_x^-$ )

fragments are regarded as indicators for oxygen-involving degradation.<sup>[13,17,20,21]</sup> As shown in Figure 4c, d, in contrast to  $\text{S}_x^-$  and  $\text{Cl}^-$  signals, higher normalized intensities for  $\text{PO}_3^-$  and  $\text{SO}_3^-$  fragments were observed on the surface of the  $\text{Li}_6\text{PS}_4\text{Cl}/\text{NCM}$  electrode. This result indicates that less solid oxygenated sulfur and phosphorus species form at the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}/\text{NCM}$  interface. Below, we propose a mechanism to explain these results in more detail.

In order to verify the above surface analytical results, additional post mortem ToF-SIMS analyses were conducted at  $45^\circ$  FIB crater sidewalls. Figure 5a displays exemplary secondary ion (SI) images of two composite cathodes after 100 cycles.  $\text{NiO}_2^-$  and  $\text{Cl}^-$  signals were used to distinguish the cathode active material and the electrolyte particles, respectively. For interfacial degradation, phosphate ( $\text{PO}_x^-$ ), sulfate/sulfite ( $\text{SO}_x^-$ ) and polysulfide ( $\text{S}_x^-$ ) signals represent different degradation processes at the SE|NCM interface. To eliminate the mass interference and maintain the lateral



**Figure 4.** Box plots of normalized a)  $\text{S}^-$  and b)  $\text{Cl}^-$  signal intensities from ToF-SIMS surface analyses of SE/NCM85 electrodes after aging at 3.7 V (vs. In/InLi) for 60 h. The signal intensities in (a) and (b) are normalized in relation to the total ion signal intensity of the corresponding spectrum. Because we assume that the oxygen-involving degradation chemical degradation exclusively takes place on the surface of the NCM secondary particles, the signal intensities of  $\text{PO}_3^-$  and  $\text{SO}_3^-$  fragments in (c) and (d) are normalized by the  $\text{NiO}_2^-$  signal intensity of the corresponding spectrum. In this way, deviations due to a different fraction of interfaces within the analysis area are partly compensated.



**Figure 6.** Voltage profile of a)  $\text{Li}_6\text{PS}_5\text{Cl}$  and b)  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cells cycled at C/20 rate and 45 °C, together with the corresponding time-resolved evolution rate (left y-axis) and cumulative gas evolution (right y-axis) for  $\text{O}_2$  and the normalized ion currents for  $\text{SO}_2$ .

resolution,  $\text{PO}_x^-$  and  $\text{SO}_x^-$  fragments were normalized by multiplication (i.e.,  $\text{PO}_2^-\cdot\text{PO}_3^-$ ,  $\text{SO}_2^-\cdot\text{SO}_3^-$ ).<sup>[13,20]</sup> To enhance the signal intensity of polysulfide fragments ( $\text{S}_x^-$ ), the images of  $\text{S}_4^-$ ,  $\text{S}_5^-$  and  $\text{S}_6^-$  were summed (see Supporting Information).

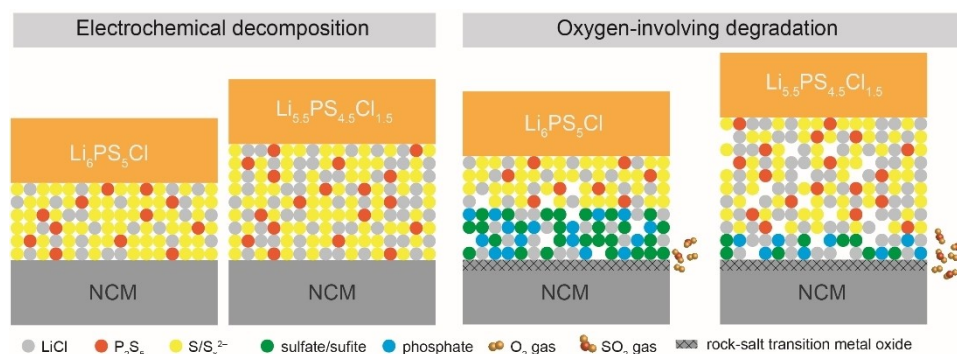
As shown in the overlay RGB image in Figure 5,  $\text{PO}_x^-$  and  $\text{SO}_x^-$  products form at the inner degradation layer (close to NCM particles), while  $\text{S}_x^-$  species form at the outer degradation layer (close to electrolyte particles). In addition to a diffusion-controlled solid-state reaction between the NCM and the SE, oxygen release from the NCM and decomposition of  $\text{Li}_2\text{CO}_3$  at high voltages (i.e., >4.2 V vs.  $\text{Li}^+/\text{Li}$ ) likely cause this inner degradation layer. In contrast, the outer degradation layer is dominated by the electrochemical decomposition reactions of the SEs (i.e., “delithiation”). After long-term cycling, both electrochemical decomposition and chemical degradation contribute to the interfacial resistance, and further voltage polarization.

Figure S11 shows the semi-quantitative results of SIMS crater wall image ROI analysis, which verifies the ToF-SIMS surface analysis shown in Figure 4. Compared with  $\text{Li}_6\text{PS}_5\text{Cl}$ ,  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows a higher normalized intensity of ( $\text{S}_4^- + \text{S}_5^- + \text{S}_6^-$ ) and a decrease in the normalized intensity

of ( $\text{PO}_2^-\cdot\text{PO}_3^-$ ). For ( $\text{SO}_2^-\cdot\text{SO}_3^-$ ); the approximately equal intensities in the two electrodes can be attributed to partially reversible redox behavior of related degradation products.<sup>[16c]</sup> At the same time,  $\text{SO}_x^-$  fragments suffer from more pronounced mass interferences with neighboring signals and low signal intensities compared to  $\text{PO}_x^-$  fragments.

In an attempt to further investigate the oxygen-involving degradation processes at the SE|NCM85 interface, in situ gassing studies via DEMS were performed. The evolved gaseous degradation products could help to elucidate possible degradation mechanisms at the SE|NCM85 interface during cycling. To this end, the cells were cycled at a rate of 0.05 C and 45 °C in the voltage range of 2–3.9 V vs. In/InLi (Figure 6). The  $\text{Li}_6\text{PS}_5\text{Cl}$  cell achieved a first cycle charge and discharge capacity of 243  $\text{mAh g}_{\text{NCM}}^{-1}$  and 201  $\text{mAh g}_{\text{NCM}}^{-1}$ , respectively. The  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell exhibited a first cycle charge and discharge capacity of 239 and 176  $\text{mAh g}_{\text{NCM}}^{-1}$ . Note that these two cells were chosen due to their relative similar initial charge capacities. Accordingly, the total amount of gas evolution from both SEs could be compared. The gas evolution was monitored within  $m/z = 1$ –100 and four main gases were detected ( $\text{H}_2$  ( $m/z = 2$ ),  $\text{CO}_2$  ( $m/z = 44$ ),  $\text{O}_2$  ( $m/z = 32$ ) and  $\text{SO}_2$  ( $m/z = 64$ )). The evolution of two gases is of major interests in this study, namely of  $\text{O}_2$  and  $\text{SO}_2$ , which will be discussed below. The evolution of  $\text{H}_2$  and  $\text{CO}_2$  gases is discussed in the Supporting Information (Figure S12).

The  $\text{O}_2$  gas evolution ( $m/z = 32$ ) is characteristic for layered Ni-rich oxides CAMs. In the case of NCM85, cells are required to achieve a state of charge (SOC) >80 %<sup>[19b,22]</sup> and this condition is met for both cells with SOC ca. 84.3 % and 82.5 % for the  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell, respectively. The origin of  $\text{O}_2$  evolution in layered Ni-rich oxides is a consequence of the destabilization of the crystalline lattice at high voltage (>4.2 V vs.  $\text{Li}^+/\text{Li}$ ).<sup>[22a,b]</sup> Moreover, the amount of  $\text{O}_2$  evolved scales exponentially with the lattice destabilization and hence the SOC. With similar charge capacities of the two cells, the cumulative amount of  $\text{O}_2$  evolved from both cells is similar (6.7  $\mu\text{mol g}_{\text{NCM}}^{-1}$  for the  $\text{Li}_6\text{PS}_5\text{Cl}$  cell and 6.8  $\mu\text{mol g}_{\text{NCM}}^{-1}$  for the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell). In addition to the  $\text{O}_2$  signal, we monitored the  $\text{SO}_2$  gas



**Figure 7.** Schematic illustration of SE|NCM interfacial degradation. At low voltages (<4.2 V vs.  $\text{Li}^+/\text{Li}$ ), the electrochemical decomposition of Li argyrodites takes place. In the high voltage range ( $\geq 4.2$  V vs.  $\text{Li}^+/\text{Li}$ ), the oxygen-involving degradation dominates the interfacial reactions, and generates gaseous (represented by  $\text{SO}_2$ ) and oxygenated sulfur and phosphorus species (sulfate/sulfite and phosphate) at the interface.



evolution ( $m/z=64$ ) simultaneously.  $\text{SO}_2$  gas evolution is commonly observed for SSB cells containing lithium thiophosphate SEs and indicates oxygen-involving degradation at the SE|CAM interface. Interestingly, the  $\text{SO}_2$  gas ion current signal for the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell had higher intensity compared to the  $\text{Li}_6\text{PS}_5\text{Cl}$  cell. This observation suggests that the formation of gaseous products from oxygen-involving degradation is increased for the  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  cell.<sup>[19b, 22c, 23]</sup>

On the basis of the ToF-SIMS and DEMS results, we propose that the oxygen-involving degradation at the SE|CAM interface leads to either gaseous (indicated by  $\text{SO}_2$  evolution (DEMS)) or solid products (indicated by  $\text{PO}_x^-$  and  $\text{SO}_x^-$  fragments (ToF-SIMS)). The mechanism of interfacial oxygen-involving degradation is rather complex, and the difference in gaseous or solid products remains unclear, which needs further investigation. Modifying the Li argyrodite SEs by halide substitution changes the fraction of gaseous and solid interfacial products which in turn influences the SSB performance.

Upon substitution of  $\text{S}^{2-}$  with  $\text{Cl}^-$ , the enhanced  $\text{Li}^+$  mobility leads to a higher ionic conductivity for Cl-rich argyrodite. However, the lower thermodynamic stability of  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  triggers a higher fraction of electrochemical decomposition in SE/C and SE/NCM electrodes (Figure 1 and 4). The oxygen-involving interfacial reactions occur in the high voltage range ( $\geq 4.2$  V vs.  $\text{Li}^+/\text{Li}$ ), where the NCM crystal lattice is destabilized and initially inert oxygen ions in the surface layer turn reactive upon oxidation. As a result, interdiffusion and solid-state reactions can occur on the one hand, and highly reactive oxygen species (i.e., singlet oxygen) can be released from the NCM lattice on the other hand, which can then further react with the SE and interfacial species. The oxygen-involving degradation at SE|NCM interface ultimately leads to gaseous species such as  $\text{SO}_2$ <sup>[23]</sup> and solid oxygenated phosphorous and sulfur species (e.g., phosphates and sulfates/sulfites).<sup>[17, 18b]</sup> Our results demonstrate that the basic reactions of the different thiophosphate-based SEs with NCM are similar, but the fractions of degradation products are different, which could be attributed to the different stoichiometric ratio of  $\text{S}_x^0$ ,  $\text{P}_2\text{S}_5$  and LiCl-related species. Accordingly, ToF-SIMS results confirm that  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  forms less solid oxygenated phosphorous and sulfur species during battery cycling compared to  $\text{Li}_6\text{PS}_5\text{Cl}$ . DEMS analysis indicates that  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  generates more gaseous degradation products such as  $\text{SO}_2$  during charging (Figure 7). Future studies may need to investigate the degradation products in more detail. Hence, the thermodynamic and kinetic properties of Li argyrodites play a significant role in driving the SE/CAM interfacial degradation.

## Conclusion

In summary, we investigated the influence of argyrodite modification on the interfacial reaction of NCM and SE. For argyrodite modification, the halide content affects the ionic conductivity by introducing  $\text{Li}^+$  vacancies and  $\text{Cl}^-/\text{S}^{2-}$  site

disorder, while it shows a complex influence on the interfacial degradation in the composite cathodes.  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows a higher fraction of electrochemical decomposition at low voltages compared to  $\text{Li}_6\text{PS}_5\text{Cl}$ . At high voltages (i.e.,  $>4.2$  V vs.  $\text{Li}^+/\text{Li}$ ),  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$  shows a higher fraction of  $\text{SO}_2$  gas evolution, but less solid oxygenated phosphorous and sulfur species (e.g., phosphates and sulfates/sulfites). Since the fraction of solid oxygenated degradation products in the interfacial region is reduced, and thus the interfacial resistance is lower, the overall cell performance is enhanced for  $\text{Li}_{5.5}\text{PS}_{4.5}\text{Cl}_{1.5}$ . By and large, this study shows that the composition and structure of the SE affect the electrochemical decomposition behavior as well as the interfacial reaction between SE and NCM. Thus, new electrolytes, which may in situ form a homogeneous lithium phosphate/phosphite or lithium sulfate/sulfite layer are promising for the modification of new electrolytes. These results highlight the possibility of solving interfacial problems through the targeted modification/development of SEs.

## Acknowledgements

This work was supported by the joint project InCa/InCa2 (projects 03XP0228C, 03XP0472A, 03XP0472B) within the German-Japanese cooperation program of BMBF (Federal Ministry for Education and Research) and NEDO (New Energy and Industrial Technology Development Organization), and the projects 03XP0177A and 03XP0430A within the Cluster of Competence FESTBATT funded by BMBF. LFN gratefully acknowledges support from NSERC via a Canada Research Chair and the Discovery Grant program. LFN also acknowledges support through her Liebig professorship at JLU. Open Access funding enabled and organized by Projekt DEAL.

## Conflict of Interest

The authors declare no competing financial interests.

## Data Availability Statement

The data that support the findings of this study are available from the corresponding author upon reasonable request.

**Keywords:** Composite Cathode • Interfacial Stability • Lithium Argyrodite Electrolyte • Solid State Battery

- [1] a) J. Janek, W. G. Zeier, *Nat. Energy* **2016**, *1*, 16141; b) J. B. Goodenough, Y. Kim, *Chem. Mater.* **2010**, *22*, 587–603; c) A. M. Bates, Y. Preger, L. Torres-Castro, K. L. Harrison, S. J. Harris, J. Hewson, *Joule* **2022**, *6*, 742–755.
- [2] a) Y. Kato, S. Hori, R. Kanno, *Adv. Energy Mater.* **2020**, *10*, 2002153; b) K. H. Park, Q. Bai, D. H. Kim, D. Y. Oh, Y. Zhu, Y. Mo, Y. S. Jung, *Adv. Energy Mater.* **2018**, *8*, 1800035; c) S. Xin, Y. You, S. Wang, H.-C. Gao, Y.-X. Yin, Y.-G. Guo, *ACS*

- Energy Lett.* **2017**, *2*, 1385–1394; d) Y. Zhu, X. He, Y. Mo, *ACS Appl. Mater. Interfaces* **2015**, *7*, 23685–23693.
- [3] a) K. Ohara, A. Mitsui, M. Mori, Y. Onodera, S. Shiotani, Y. Koyama, Y. Orikasa, M. Murakami, K. Shimoda, K. Mori, T. Fukunaga, H. Arai, Y. Uchimoto, Z. Ogumi, *Sci. Rep.* **2016**, *6*, 21302; b) F. Mizuno, A. Hayashi, K. Tadanaga, M. Tatsumisago, *Adv. Mater.* **2005**, *17*, 918–921.
- [4] a) T. Krauskopf, S. P. Culver, W. G. Zeier, *Chem. Mater.* **2018**, *30*, 1791–1798; b) D. A. Weber, A. Senyshyn, K. S. Weldert, S. Wenzel, W. Zhang, R. Kaiser, S. Berendts, J. Janek, W. G. Zeier, *Chem. Mater.* **2016**, *28*, 5905–5915; c) N. Kamaya, K. Homma, Y. Yamakawa, M. Hirayama, R. Kanno, M. Yone-mura, T. Kamiyama, Y. Kato, S. Hama, K. Kawamoto, A. Mitsui, *Nat. Mater.* **2011**, *10*, 682–686.
- [5] Y. Kato, S. Hori, T. Saito, K. Suzuki, M. Hirayama, A. Mitsui, M. Yonemura, H. Iba, R. Kanno, *Nat. Energy* **2016**, *1*, 16030.
- [6] a) C. Yu, S. Ganapathy, J. Hageman, L. van Eijck, E. R. H. van Eck, L. Zhang, T. Schwietert, S. Basak, E. M. Kelder, M. Wagemaker, *ACS Appl. Mater. Interfaces* **2018**, *10*, 33296–33306; b) N. Minafra, S. P. Culver, T. Krauskopf, A. Senyshyn, W. G. Zeier, *J. Mater. Chem. A* **2018**, *6*, 645–651; c) M. A. Kraft, S. P. Culver, M. Calderon, F. Bocher, T. Krauskopf, A. Senyshyn, C. Dietrich, A. Zevalkink, J. Janek, W. G. Zeier, *J. Am. Chem. Soc.* **2017**, *139*, 10909–10918.
- [7] a) Y. Xiao, L. J. Miara, Y. Wang, G. Ceder, *Joule* **2019**, *3*, 1252–1275; b) G. F. Dewald, S. Ohno, M. A. Kraft, R. Koerver, P. Till, N. M. Vargas-Barbosa, J. Janek, W. G. Zeier, *Chem. Mater.* **2019**, *31*, 8328–8337; c) T. T. Zuo, R. Ruess, R. Pan, F. Walther, M. Rohnke, S. Hori, R. Kanno, D. Schroder, J. Janek, *Nat. Commun.* **2021**, *12*, 6669.
- [8] a) G. Xu, L. Luo, J. Liang, S. Zhao, R. Yang, C. Wang, T. Yu, L. Wang, W. Xiao, J. Wang, J. Yu, X. Sun, *Nano Energy* **2022**, *92*, 106674; b) L. Zhou, T.-T. Zuo, C. Y. Kwok, S. Y. Kim, A. Assoud, Q. Zhang, J. Janek, L. F. Nazar, *Nat. Energy* **2022**, *7*, 83–93; c) L. Zhou, C. Y. Kwok, A. Shyamsunder, Q. Zhang, X. Wu, L. F. Nazar, *Energy. Environ. Sci.* **2020**, *13*, 2056–2063.
- [9] a) X. T. Bai, Y. Duan, W. D. Zhuang, R. Yang, J. T. Wang, *J. Mater. Chem. A* **2020**, *8*, 25663–25686; b) M. Ghidui, J. Ruhl, S. P. Culver, W. G. Zeier, *J. Mater. Chem. A* **2019**, *7*, 17735–17753.
- [10] A. Gautam, M. Sadowski, M. Ghidui, N. Minafra, A. Senyshyn, K. Albe, W. G. Zeier, *Adv. Energy Mater.* **2021**, *11*, 2003369.
- [11] a) P. Adeli, J. D. Bazak, K. H. Park, I. Kochetkov, A. Huq, G. R. Goward, L. F. Nazar, *Angew. Chem. Int. Ed.* **2019**, *58*, 8681–8686; *Angew. Chem.* **2019**, *131*, 8773–8778; b) C. Yu, Y. Li, M. Willans, Y. Zhao, K. R. Adair, F. Zhao, W. Li, S. Deng, J. Liang, M. N. Banis, R. Li, H. Huang, L. Zhang, R. Yang, S. Lu, Y. Huang, X. Sun, *Nano Energy* **2020**, *69*, 104396.
- [12] D. H. S. Tan, E. A. Wu, H. Nguyen, Z. Chen, M. A. T. Marple, J.-M. Dour, X. Wang, H. Yang, A. Banerjee, Y. S. Meng, *ACS Energy Lett.* **2019**, *4*, 2418–2427.
- [13] F. Walther, R. Koerver, T. Fuchs, S. Ohno, J. Sann, M. Rohnke, W. G. Zeier, J. Janek, *Chem. Mater.* **2019**, *31*, 3745–3755.
- [14] A. Schürmann, B. Luerßen, D. Mollenhauer, J. Janek, D. Schröder, *Chem. Rev.* **2021**, *121*, 12445–12464.
- [15] F. Strauss, J. H. Teo, J. Maibach, A. Y. Kim, A. Mazilkin, J. Janek, T. Brezesinski, *ACS Appl. Mater. Interfaces* **2020**, *12*, 57146–57154.
- [16] a) D. Park, H. Park, Y. Lee, S. O. Kim, H. G. Jung, K. Y. Chung, J. H. Shim, S. Yu, *ACS Appl. Mater. Interfaces* **2020**, *12*, 34806–34814; b) Y. Xiao, Y. Wang, S.-H. Bo, J. C. Kim, L. J. Miara, G. Ceder, *Nat. Rev. Mater.* **2019**, *5*, 105–126; c) J. Auvergniot, A. Cassel, J.-B. Ledeuil, V. Viallet, V. Seznec, R. Dedryvère, *Chem. Mater.* **2017**, *29*, 3883–3890.
- [17] F. Walther, S. Randau, Y. Schneider, J. Sann, M. Rohnke, F. H. Richter, W. G. Zeier, J. Janek, *Chem. Mater.* **2020**, *32*, 6123–6136.
- [18] a) W. Zhang, F. H. Richter, S. P. Culver, T. Leichtweiss, J. G. Lozano, C. Dietrich, P. G. Bruce, W. G. Zeier, J. Janek, *ACS Appl. Mater. Interfaces* **2018**, *10*, 22226–22236; b) W. Zhang, D. A. Weber, H. Weigand, T. Arlt, I. Manke, D. Schröder, R. Koerver, T. Leichtweiss, P. Hartmann, W. G. Zeier, J. Janek, *ACS Appl. Mater. Interfaces* **2017**, *9*, 17835–17845; c) M. D. Levi, D. Aurbach, *J. Phys. Chem. B* **1997**, *101*, 4630–4640; d) J. Moškon, M. Gaberšček, *J. Power Sources Adv.* **2021**, *7*, 100047; e) J. Moškon, J. Žuntar, S. Drvarič Talian, R. Dominko, M. Gaberšček, *J. Electrochem. Soc.* **2020**, *167*, 140539.
- [19] a) G. L. Xu, X. Liu, A. Daali, R. Amine, Z. Chen, K. Amine, *Adv. Funct. Mater.* **2020**, *30*, 2004748; b) F. Strauss, J. H. Teo, A. Schiele, T. Bartsch, T. Hatsukade, P. Hartmann, J. Janek, T. Brezesinski, *ACS Appl. Mater. Interfaces* **2020**, *12*, 20462–20468.
- [20] F. Walther, F. Strauss, X. Wu, B. Mogwitz, J. Hertle, J. Sann, M. Rohnke, T. Brezesinski, J. Janek, *Chem. Mater.* **2021**, *33*, 2110–2125.
- [21] Y. Yamagishi, H. Morita, Y. Nomura, E. Igaki, *ACS Appl. Mater. Interfaces* **2021**, *13*, 580–586.
- [22] a) R. Jung, M. Metzger, F. Maglia, C. Stinner, H. A. Gasteiger, *J. Electrochem. Soc.* **2017**, *164*, A1361–A1377; b) R. Jung, P. Strobl, F. Maglia, C. Stinner, H. A. Gasteiger, *J. Electrochem. Soc.* **2018**, *165*, A2869–A2879; c) T. Bartsch, F. Strauss, T. Hatsukade, A. Schiele, A. Y. Kim, P. Hartmann, J. Janek, T. Brezesinski, *ACS Energy Lett.* **2018**, *3*, 2539–2543.
- [23] J. H. Teo, F. Strauss, Đ. Tripković, S. Schweidler, Y. Ma, M. Bianchini, J. Janek, T. Brezesinski, *Cell Rep. Phys. Sci.* **2021**, *2*, 100465.

Manuscript received: September 7, 2022

Accepted manuscript online: November 23, 2022

Version of record online: January 10, 2023